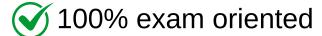


# STUDY MATERIAL FOR BOILER OPERATION ENGINEER EXAMS









# **MORE INFO**



# **NUMERICALS FROM BOE EXAMS**

#### PROPERTIES OF STEAM

# Problem (Maharashtra BOE 2014, 2024, 6 marks)

Find the volume of 1 kg of steam at pressure of  $14 \text{ kg/cm}^2(g)$  in each of the following case:

- (i) When steam is dry saturated?
- (ii) When steam is wet having dryness fraction 0.9?
- (iii) When steam is superheated, the degree of superheat being  $40^{\circ}C$ ?

#### Solution

$$\begin{split} P_{abs} &= P_g + P_{atm} \\ &= 14 + 1.033 = 15.033 \; kg/cm^2 \; say \; 15 \; kg/cm^2 \end{split}$$

From steam tables at  $P_{abs} = 15 \text{ kg/cm}^2$ 

Specific volume of dry saturated steam

$$v_g = 0.1317 \text{ m}^3/\text{kg}$$

Volume of dry saturated steam

$$V_{dry} = mv_g = 1 \text{ kg x } 0.1317 \text{ m}^3/\text{kg} = 0.1317 \text{ m}^3$$

Specific volume of wet steam

$$v_{wet} = xv_g$$
 
$$v_{wet} = 0.9 \times 0.1317 \text{ m}^3/\text{kg} = 0.1153 \text{ m}^3/\text{kg}$$

Volume of wet steam

$$V_{wet} = mv_{wet} = 1 \ kg \ x \ 0.1153 \ m^3/kg = 0.11853 \ m^3$$

From steam tables for  $P_{abs}=15\ kg/cm^2,$  the saturation temperature is  $T_{sat}=198.3^{0}C$ 

Superheated temperature

$$\begin{split} T_{sup} &= T_{sat} + \Delta T_{sup} \\ &= 198.3^{0}C + 40^{0}C = 238.3^{0}C \end{split}$$

From superheated steam tables at  $P_{abs} = 15 \text{ kg/cm}^2$  and  $T_{sup} = 283.3^{\circ}\text{C}$ ,

specific volume,  $v_{sup} = 0.153 \text{ m}^3/\text{kg}$ 

Volume of superheated steam

$$V_{sup} = mv_{sup} = 1 \text{ kg x } 0.153 \text{ m}^3/\text{kg} = 0.153 \text{ m}^3$$

# Problem (Gujarat BOE 2023, 5 marks)

Calculate amount of heat required to produce 5 Kg of steam at pressure 5 Bar. Feed water temperature is  $20^{0}$ C & steam is dry saturated. (Gujarat BOE 2023, 5 marks)

#### Solution

Given data

$$p = 5 bar$$

$$t_{\rm w} = 25^{0} \rm C$$

From steam tables, corresponding to pressure of 5 bar

Abs. Pressure	Temp.	Sp. enthalpy			
bar	<b>0</b> С		(kJ/kg)		
p	$t_{\rm s}$	$h_{\rm f}$	h <sub>fg</sub>	hg	
5.0	151.8	640.1	2107.4	2747.5	
5.2	153.3	646.5	2102.7	2749.3	

$$h_f = 640.1 \text{ kJ/kg}$$

$$h_{fg}=2107.4\;kj/kg$$

$$t = 151.8$$
  $^{0}C$ 

Water temperature =  $20^{\circ}$ C

Heat already in water =  $4.2 \times 20 = 84 \text{ kJ}$ 

When the steam is dry saturated

We know that enthalpy or total heat of 1 kg of dry saturated steam

$$h_g = h_f + h_{fg} = 640.1 + 2107.4 = 2747.5 \text{ kJ}$$

Hence, heat actually required = 2747.5 - 84 = 2663.5 kJ

# Problem (Gujarat BOE 2021, 2024, 5 marks)

Steam is generated in a boiler at  $110 \text{ kg/cm}^2$  at  $520^{0}\text{C}$ . Assume drum pressure is  $118 \text{ kg/cm}^2$ . Using steam table, find:

- 1. Saturated steam temperature.
- 2. Degree of superheat.
- 3. Enthalpy of steam.

#### **Solution**

(i) From the steam table, saturated temperature corresponding to  $118 \text{ kg/cm}^2$  (=118/1.02 = 116 bar) (drum pressure) is 322 °C.

Absolute pressure (bar)	Temp.	Specific enthalpy (kJ/kg)		Specific entropy (kJ/kg K)			Specific volume (m³/kg)		
P	$t_s$	$h_f$	$h_{fg}$	$h_{g}$	$s_f$	s <sub>fg</sub>	Sg	$v_f$	$v_{g}$
110.0	318.0	1 450.6	1 258.7	2 709.3	3.4304	2.1291	5.5595	0.001488	0.0160
112.0	319.4	1 458.9	1246.5	2705.4	3.4440	2.1036	5.5476	0.001496	0.0157
114.0	320.7	1467.2	1234.3	2 701.5	3.4574	2.0783	5.5357	0.001504	0.0153
116.0	322.1	1475.4	1 222.0	2697.4	3.4708	2.0531	5.5239	0.001511	0.0149
118.0	323.4	1483.6	1 209.7	2 693.3	3.4840	2.0280	5.5121	0.001519	0.0146

(ii) Degree of super heat = Superheated steam temperature – Saturated temperature

$$= 520 - 322 = 198$$
 °C.

(iii) Enthalpy of the superheated steam as found from steam table corresponding to  $110 \text{ kg/cm}^2$  (=110/1.02 = 108 bar) and 520 °C is 815.8 kcal/kg.

$\downarrow p (bar)$ $(t_s)$	<i>t</i> (°C) →	350	375	400	450	500	550	600	700
80	v	0.02995	0.03222	0.03432	0.03817	0.04175	0.04516	0.04845	0.05481
(294.9)	h	2987.3	3066.1	3138.3	3272.0	3398.3	3521.0	3642.0	3882.4
	s	6.130	6.254	6.363	6.555	6.724	6.878	7.021	7.281
90	v	0.0258	0.02796	0.02993	0.03350	0.03677	0.03987	0.04285	0.04857
(303.3)	h	2956.6	3041.3	3117.8	3256.6	3386.1	3511.0	3633.7	3876.5
	s	6.036	6.169	6.285	6.484	6.658	6.814	6.959	7.222
100	v	0.02242	0.02453	0.02641	0.02975	0.03279	0.03564	0.03837	0.04358
(311.0)	h	2923.4	3015.4	3096.5	3240.9	3373.7	3500.9	3625.3	3870.5
	s	5.944	6.089	6.212	6.419	6.597	6.756	6.903	7.169
110	v	0.01961	0.02169	0.02351	0.02668	0.02952	0.03217	0.03470	0.03950
(318.0)	h	2887.3	2988.2	3074.3	3224.7	3361.0	3490.7	3616.9	3864.5
	s	5.853	6.011	6.142	6.358	6.540	6.703	6.851	7.120

# Problem (Gujarat BOE 2023, 5 marks)

Steam at  $100^{\circ}$ C is added to ice at  $0^{\circ}$ C. Find the amount of ice melted and the final temperature when mass of steam is 10.0 grams and the mass of ice is 50.0 grams.

#### Solution

$$m_{ice} = \frac{m_{steam} L_{steam} + m_w C_w \Delta T}{L_{ice}}$$
$$= \frac{10(540) + (1)(1)(100 - 0)}{80} = 68.75 g$$

68.75 g > 50 g

Hence, entire ice will melt.

Hence, final temperature will be  $0^{\circ}$ C.

# Problem (Gujarat BOE 2021, 5 marks0

Calculate the heat required to be added to 1000 kg of steam at 15 kg/cm<sup>2</sup> in order to superheat to 400 centigrade.

### **Solution**

 $m_{steam} = 1000 \text{ kg}$ 

 $P_{\text{steam}} = 15 \text{ kg/cm}^2$ 

Final temperature of superheated steam,  $T_2 = 400^{\circ}$ C

Saturation temperature of steam at  $15 \text{ kg/cm}^2 = 198.3^{\circ}\text{C}$ 

Specific heat capacity of superheated steam,  $C_p = 2.09 \text{ kJ/kg}^0\text{C}$ 

$$\Delta T = 400 - 198.3 = 201.7^{\circ}C$$

Now using

$$Q = mC_p \Delta T = 1000 \text{ x } 2.09 \text{ x } 201.7 = 421543 \text{ kJ}$$

# Problem (Maharashtra BOE 2023, 6 marks)

What quantity of heat is required to raise the temperature of 450 grams of water from 15°C to 85°C? The specific heat capacity of water is 4.18 J/g/°C.

#### Solution

$$Q = mc\Delta T = (450 \text{ g})(4.18 \text{ J/g/}^{0}\text{C})(85 - 15) = 131670 \text{ J}$$

# Problem (Gujarat BOE 2021, 5 marks)

Find suitable size of pipe to carry 320 tons of steam per hour with specific volume of 0.22  $m^3/kg$  at approximately 40 m/sec velocity. (Gujarat BOE 2021, 5 marks)

#### Solution

Mass flow rate of steam = 320 t/hr = 88.89 kg/s

Sp. volume of steam =  $0.22 \text{ m}^3/\text{kg}$ 

Velocity of steam = 40 m/s

Now, Q = mass flow rate x specific volume

$$= 88.89 \times 0.22 = 19.556 \text{ m}^3/\text{s}$$

Now area 
$$A = Q/\text{velocity} = 19.556/40 = 0.4889 \text{ m}^2$$

$$A = \frac{\pi D^2}{4}$$

Hence 
$$0.4889 = \frac{\pi D^2}{4}$$

Giving 
$$D = 0.788 \text{ m}$$

# FUELS, COMBUSTION AND FLUE GASES

# Problem (Karnataka BOE 2023, 5 marks)

If one ball of coal of 250 c.c. volume breaks in to small 250 pcs. of ball having a volume of 1 cc of each ball, calculate how many times the surface area exposed to heat for combustion will increase?

#### Solution

**Volume** 
$$V_L = \frac{4}{3}\pi r_L^3 \Rightarrow 250 = \frac{4}{3}r_L^3 \Rightarrow r_L = \left(\frac{750}{4\pi}\right)^{1/3} cm$$

$$1 = \frac{4}{3}\pi r_S^3 \Rightarrow r_s = \left(\frac{3}{4\pi}\right)^{1/3} cm$$
 [ Volume of one ball = 250/250 = 1 cc]

Now area 
$$A_L = 4\pi \left[ \left( \frac{750}{4\pi} \right)^{1/3} \right]^2 = 4\pi \left( \frac{750}{4\pi} \right)^{2/3} cm^2$$

$$A_{S} = 4\pi \left[ \left( \frac{3}{4\pi} \right)^{1/3} \right]^{2} = 4\pi \left( \frac{3}{4\pi} \right)^{2/3} cm^{2}$$

**Ratio** 

$$\frac{A_{S,total}}{A_L} = \frac{250(4\pi) \left(\frac{3}{4\pi}\right)^{2/3}}{4\pi \left(\frac{750}{4\pi}\right)^{2/3}} = 6.3$$

# Problem (Assam BOE 2023, 2 marks)

Fuel oil-fired boiler's steam rate averages 114 lb of steam/gal. of fuel oil. The boiler operates 24 hr/day, 350 days/yr. The fuel oil costs ₹1.75/gal. and the load is 50 Klb/hr. What is the annual fuel cost?

# **Solution**

FC= (Fuel oil cost x 24 x 350 x load)/Steam rate

 $= (1.75 \times 24 \times 350 \times 50,000)/1.75$ 

= ₹ 42,00,00,000

# Problem (Gujarat BOE 2023, 5 marks)

Following parameters are noted from the ultimate analysis of coal sample:

Carbon: 40%

Sulphur: 2%

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Hydrogen: 4%

Calculate the theoretical quantity of air required in kilograms. If the boiler is operated at 4% excess oxygen, then calculate the actual air quantity in kilograms.

#### Solution

#### Theoretical air

Method 1

Constituent	Mass	Mass of O <sub>2</sub> required	Mass of products (k		cts (kg)
	fraction	for complete combustion	N <sub>2</sub>	CO <sub>2</sub>	SO <sub>2</sub>
С	0.4	$0.4 \times (8/3) = 1.07$		0.4 x (11/3)	
				= 1.47	
$H_2$	0.04	$0.04 \times 8 = 0.32$			
S	0.02	0.02 x 1= 0.02			0.02 x 2
					= 0.04
Total		$\Sigma = 1.41$		$\Sigma = 1.47$	$\Sigma = 0.02$
$O_2$	0	0			

|--|

Total  $O_2$  required for complete combustion = 1.41 - 0 = 1.41 kg/kg of fuel

Air required =  $1.41 \times (100/23) = 6.12 \text{ kg/kg}$  of fuel

Method 2

Quantity of theoretical air required (by weight) per kilogramme of fuel is given by

$$4.35 \left[ \left( \frac{8}{3}C + 8H_2 + S \right) - O_2 \right] kg$$
$$= 4.35 \left( \frac{8}{3}x0.4 + 8x0.04 + 0.02 \right) = 6.12 kg$$

# **Actual air quantity**

Excess air percentage = 
$$\frac{Oxygen\ percentage\ in\ flue\ gas}{21 - Oxygen\ percentage} x100$$

Boiler is operated at 4% excess oxygen.

Hence, excess air percentage = 
$$\frac{4}{21-4} \times 100 = 23.5\%$$

Actual air qty = Theoretical air 
$$\left(1 + \frac{excess air\%}{100}\right)$$
  
= 6.12 x 1.235 = 7.35 kg/kg of fuel

# Problem (Chhattisgarh BOE 2021, 5 marks)

The following is the percentage composition of coal on mass basis:

$$H_2 = 3.3\%$$

$$O_2 - 3\%$$

$$S - 0.9\%$$

and remaining is ash.

Calculate

- (i) The theoretical air required to burn 1 kg of coal completely.
- (ii) The percentage composition of dry flue gases on mass basis if 50% excess air is supplied. Assume air has 23% oxygen on mass basis.

# **Solution**

Constituent	Mass	Mass of O <sub>2</sub> required	Mass of product		cts (kg)
	fraction	for complete combustion	N <sub>2</sub>	CO <sub>2</sub>	SO <sub>2</sub>
С	0.9	$0.9 \times (8/3) = 2.4$		0.9 x (11/3)	
				= 3.3	
H <sub>2</sub>	0.033	$0.033 \times 8 = 0.264$			
S	0.009	0.009 x 1= 0.009			0.009 x 2
					= 0.018
Total		$\Sigma = 2.673$		$\Sigma = 3.3$	$\Sigma = 0.08$
$O_2$	0.03	0.03			
$N_2$	0		0		

Total  $O_2$  required for complete combustion = 2.673 - 0.03 = 2.643 kg/kg of fuel

Air required =  $2.643 \times (100/23) = 11.49 \text{ kg/kg of fuel}$ 

# For 50% air

$$N_2 = 11.49 \text{ x } 1.5 \text{ x } 0.77 + 0 = 13.27 \text{ kg}$$
  
 $O_2 = 11.49 \text{ x } 0.5 \text{ x } 0.23 = 1.32 \text{ kg}$ 

Constituent	Mass (kg)	% by mass
CO <sub>2</sub>	3.3	3.3 x (100/17.908) = 18.43
SO <sub>2</sub>	0.018	$0.018 \times (100/17.908) = 0.10$
N <sub>2</sub>	13.27	13.27 x (100/17.908) = 74.10
$O_2$	1.32	1.32 x (100/17.908) = 7.37
	$\Sigma = 17.908$	

# **Problem (Jharkhand BOE 2022, 4 marks)**

Estimate SO<sub>2</sub> emission through chimney in tons/annum.

Data:

 $Days\ considered = 340$ 

 $Fuel\ used = furnace\ oil$ 

Specific gravity = 0.94

 $Sulphur\ content = 3.8\%$ 

Quantity of FO (Fuel Oil) consumption = 3.5 kl/hr

and if measured  $O_2$  in flue gas is 2.5%, find excess air level.

#### **Solution**

Quantity of sulphur/annum

$$= 3500 \times 0.94 \times 24 \times 340 \times 0.038$$

$$S + O_2 \rightarrow SO_2$$

We conclude that 1 kg of sulphur produces 2 kg of SO<sub>2</sub>.

Quantity of SO<sub>2</sub> generated per annum

$$= 2 \times 1020163.2$$

= 20403264.4 kg/annum

= 2041 tonnes/annum

For 2.5% O<sub>2</sub> in flue gas, excess air

$$= \frac{O_2}{21 - O_2} = \frac{2.5}{21 - 2.5} = 0.1351 = 13.51\%$$

# Problem (Punjab BOE 2021, 10 marks)

A sample of fuel has the following percentage composition by weight:

$$Hydrogen = 10 \%$$

$$Oxygen = 3.5\%$$

$$Nitrogen = 1.5\%$$

$$Ash = 3.5\%$$

- (i) Determine the stoichiometric air-fuel ratio by mass
- (ii) If 20% excess air is supplied, find the percentage composition of dry flue gases by volume.

#### **Solution**

#### Stoichiometric air fuel ratio

On the basis of 100 kg of fuel let us assume an equivalent formula C<sub>a</sub>H<sub>b</sub>O<sub>c</sub>N<sub>d</sub>.

From the given analysis by weight, we can write

$$12a = 84 \Rightarrow a = 7$$

$$1b = 10 \Rightarrow b = 10$$